


## Housekeeping

- Quiz answers
  - Add technical details to answers
  - Be sure you can answer last year's questions
  - Why agriculture isn't regulated
  - How it might be pushed to eco-awareness
- Change of Plans....
- How was the Municipal P2 viewing?
- State of the Art topics



	Average Scores			Max
	All	Grade	Under	
1/1/2012 Intro to P2	9.047	8.667	9.667	10
1/8/2012 Ind. Activity and Env.	10.239	10.036	10.556	10
1/25/2012 Municipal P2				10
1/31/2012 Field Trip - Cargill				10
2/1/2012 Fuel Cells, Biogas, SDA, Pumps				10
2/8/2012 Life Cycle Assessment				10
2/15/2012 Design for Env. - <b>Spiller</b>				10
2/22/2012 MSW Field Trip				10
2/29/2012 <b>P2 Economics</b>				10
3/7/2012 P2 Planning / Town Hall - <b>Legare</b>				10
3/21/2012 Energy Conservation - <b>Walton</b>				10
Field Trip - Zimmerman				10
3/28/2012 <b>Fugitive Emissions</b> - <b>Legare</b>				10
Field Trip - Recycled Materials				10
4/4/2012 P2 and BMPs in Industry				10
4/11/2012 Brewery and P2 - <b>Smith</b>				10
Field Trip - Coors				10
4/18/2012 Metals Removal				10
4/25/2012 Water Resources, DNAPLs, and Fracking				10
Personal Quiz Average				10
Total Quiz and Homework Points				150




## P2 Technologies Biogas and Fuel Cells

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Indigo Water Group 



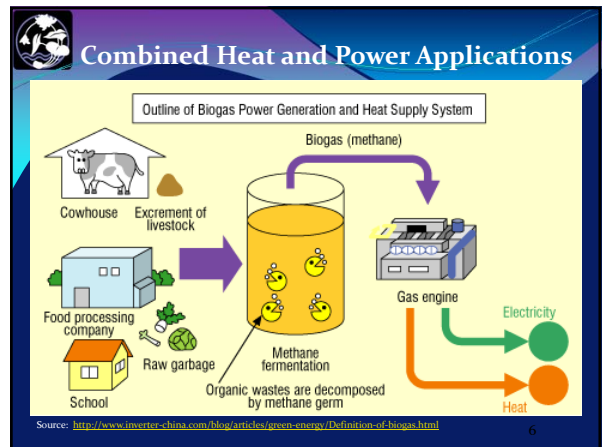
## What is Biogas and Where Does it Come From?

- A methane rich byproduct produced when organic matter breaks down anaerobically
- Sources of biogas:
  - Decomposing vegetation
  - Farm and ranch animals
  - Manure from farm and ranch animals
  - Wastewater plants
  - Landfills




## Typical Biogas Utilization

- As fuel for boilers (heat production)
- As fuel for combustion engines (electric energy production and heat recovery)
- After CO<sub>2</sub> separation, gas can be pressed into a gas grid (use like natural gas)
- Heating and cooking "off the grid"









# Anaerobic Digestion

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# Digestion Processes

- Anaerobic Digestion
  - Ponds
  - Septic Tanks
  - Engineered Systems
- Bacteria break down in **Endogenous Respiration**
- End products of digestion are carbon dioxide, water, and bits that don't degrade easily


$$C_4H_7O_2N \rightarrow CO_2 + H_2O$$


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# Anaerobic Digestion

- Absence of Oxygen and Nitrate
- Fermentation process
- Depends on two groups of bacteria
  - Acid Formers or Saprophytic Organisms
  - Methane Formers
- Generally not cost effective below 5 mgd - *changing*



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# Anaerobic Digestion

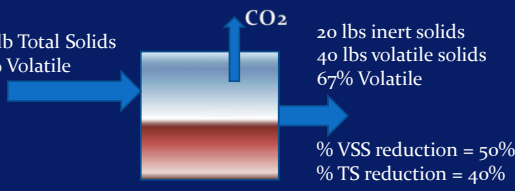
```

    graph LR
      A[Raw Sludge] -- "+" --> B[Acid Formers]
      B -- "→" --> C[Organic Acids  
CO2, H2O]
      C -- "+" --> D[Methane Formers]
      D -- "←" --> E[Methane  
CO2, H2O]
    
```

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# Volatile Solids Reduction


$$\% \text{ VSS Reduction} = \frac{(In - Out)}{In - (In * Out)} * 100$$


100 lb Total Solids  
80% Volatile

20 lbs inert solids  
40 lbs volatile solids  
67% Volatile

CO<sub>2</sub>

% VSS reduction = 50%  
% TS reduction = 40%



If MLSS is 82% volatile and solids leaving the digester are 67% volatile, find the %VSS reduction.

$$\% \text{ VSS Reduction} = \frac{(In - Out)}{In - (In * Out)} * 100$$

$$\% \text{ VSS Reduction} = \frac{(0.82 - 0.67)}{0.82 - (0.82 * 0.67)} * 100$$

$$\% \text{ VSS Reduction} = 55.4\%$$

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## Types of Anaerobic Digesters

Type	Temperature Range, °F	Solid Retention Time, days
Psychrophilic	Unheated	60+
Mesophilic	68 - 113 (95°F)	25 - 30
Thermophilic	120 - 135	5 - 12

## Anaerobic Digester Components

- Cylindrical, cubical, or egg-shaped tank
- Sloped floor (1:4 to 1:6 side slope)
- Fixed or Floating Cover
- Mixing Equipment
- Supernatant Tubes
- Sludge Draw Off Tubes
- Gas System

The diagram shows six cross-sectional views of digester covers. The top row includes 'Flat', 'Steel Truss', and 'Domed' covers, all labeled as 'Fixed Covers'. The bottom row includes 'Floating', 'Gas Holder', and 'Membrane' covers.

A collage of four photographs showing different types of anaerobic digesters: a large cylindrical tank, a floating cover with people on top, a large domed cover, and two large spherical tanks.

A photograph showing two large, dark, domed anaerobic digester tanks situated in an open field under a cloudy sky.

## Fixed Cover Tank

- Designed to maintain 8-inch water column of gas pressure on tank roof
- Occasionally designed for higher pressure
- Flat versus Domed Cover
- Can develop explosive gas mixture
  - 5 - 15% gas/air mixtures
  - Add new sludge
  - Withdraw an equal amount of supernatant or sludge
  - Maintain constant level



## Floating Cover Tank

- Cover moves up and down with tank level
- Vertical travel of 8 feet typical
- Total depth of 20 feet or more
- Stops or **Corbels** spaced every 10-16 feet around
- Roller Guides ensure even travel
- Maximum water level controlled by overflow pipe
- **Water seal** prevents air from entering tank

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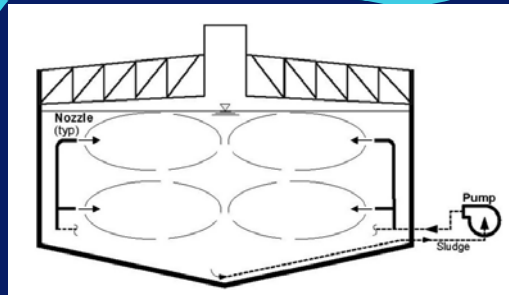
## Mixing

- Utilizes entire digester volume
- Distributes raw sludge throughout tank
- Contacts microorganisms with food
- Distributes inhibitory byproducts
- Assists with pH and alkalinity control
- Distributes heat
- Minimizes separation of grit and scum

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## Pumped Mixing for Smaller Digesters



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### Gas or Lance Mixing

### Other Types of Mixing

- Impeller Mixing
- Bubble Gun System
- Draft Tube


### Supernatant and Sludge Withdrawal Tubes

- Three to five tubes set at different depths
- Multiple lengths
- Allow operator to draw supernatant and sludge from different depths
- Some digesters use a single, adjustable tube for supernatant




### Gas System

- Digestion Process Produces
  - 8 to 12 cubic feet of gas for every lb VSS ADDED
  - 12 to 18 cubic feet of gas for every lb VSS DESTROYED
- Gas Mixture should be
  - 65 - 75 percent methane by volume
  - 30 - 35 percent carbon dioxide by volume
- Trace gases also present
  - Hydrogen, nitrogen, hydrogen sulfide, etc

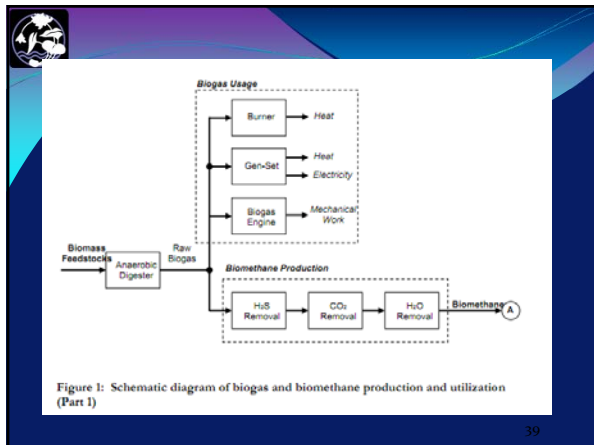



## Heating Value for Digester Gas

- 500 to 600 BTU per cubic foot
  - BTU = British Thermal Unit = Energy to raise 1 lb of water by one °F
- Natural gas has a heating value of 900 to 1,200 BTU per cubic foot
- Reuse to heat digester and/or buildings or “flare” for safety




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## Digester Heating


- Heat required to raise temperature of incoming sludge
- Heat required to make up transmission losses
- Sludge Heating Formula
  - $Q = (S)(C_s)(T_o - T_i)$
  - Q = Heat requirement in BTU/hr
  - S = Solids flow rate in lb/hr
  - Cs = Specific Heat of Solids (1 BTU / lb \* °F)
  - T = Temperature of operation and initial, °F

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## Digester Heating

- Digester gas scrubbed
- Sent to Boiler
- Recirculate digesting sludge through heat exchanger
- Internal or external to tank
- Recirculation pump keeps velocity at 4 fps to minimize fouling




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## Anaerobic Digester Operation

- Pump as thick as sludge to digester as possible
- Thin sludge is < 3.5% solids
- Excess water causes
  - Additional heating capacity to maintain temperature
  - Reduction in retention times
  - Reduces buffering capacity by forcing out supernatant
  - Increased decant frequency
- Sludge concentrations greater than 10% don't digest well


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## Anaerobic Digester Operation

- Air entering tank creates explosive gas mixture
- Adjust sludge withdrawal rate to
  - Maintain positive pressure in digester
  - Prevent vacuum formation
- Monitor Volatile Acid to Alkalinity Ratio
  - Generally less than 0.1
  - Volatile acids less than 500 mg/L
  - Problem when ratio gets to 0.5
- pH should be near 7.0 or a little higher


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## Anaerobic Digester Operation

- Loading rate of 0.15 – 0.35 lb VSS per cubic foot OR
- 150 – 300 lbs of VSS per day per 1,000 cubic feet
- Primary and secondary digesters often used
- Primary digester receives raw sludge
- Secondary digester
  - Digests at a slower rate
  - Settles digested sludge
  - Provides seed sludge for Primary when needed


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## Operating Parameter Cheat Sheet


Parameter	Units	Target
Temperature	Degrees F	90 – 100
Volatile Acids	mg/L	50 – 330
Alkalinity	Mg/L as CaCO <sub>3</sub>	1500 – 5000
VA/Alk Ratio	none	0.1 – 0.2
pH	S.U.	6.8 – 7.2
Gas Production	cf/d	12 – 16 cf/lb VS destroyed

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## Common Operational Problems

- Souring of Digester
  - Acid formers out-pace methane formers
  - Neutralize with 1 lb lime per 1,000 gallons sludge
  - Jar test for accurate dosing
- Foaming
  - Often caused by over feeding
  - Methane formers grow rapidly
  - Reduce feeding and mix gently to release gas



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## Control Strategy

- Stop or reduce solids feed
- Determine the cause of the imbalance
- Correct the cause
- Provide pH control until balance returns

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## Advantages of Anaerobic Digestion

- **Methane Gas Utilization**
- Better VS Reduction than Aerobic Digestion
- Reduces Total Solids Mass
- Good Pathogen Deactivation
- Low Net Energy Requirements
- Decreases Sludge Volume
- Less Sludge Storage Required
- Lower Annual Operating Costs



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## Anaerobic Digestion Disadvantages



- High Initial Capital Costs
- High Operator Attention
- May Experience Foaming
- Grit Removal
- Supernatant Can Have Significant Ammonia Recycle Load
- High Cleaning Cost
- Struvite Potential

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## Class "A" With Respect to Pathogens

- Fecal < 1000 MPN/g or Salmonella s.p. < 3 MPN/4g (based on seven samples per event) **AND**
- Use one of 5 approved methods to **Further Reduce Pathogens**:
  - Time/temp depending on solids content
  - pH/time then dry to at least 50% solids
  - Testing for enteric viruses/viable helminth ova
  - Testing
  - PFRP: composting, heat drying, heat treatment, TAD, beta ray irradiation, gamma ray irradiation, pasteurization, other as approved by EPA Region 8






## Class "B" With Respect to Pathogens

- 7 samples - Geometric Mean <2,000,000 MPN/g or CFU\* (based on seven samples per event) **OR**
- Use 1 of 5 Approved **Process to Significantly Reduce Pathogens (PSRP)** methods:
  - Aerobic Digestion: 40 days @ 20 C no less than 60 days @15 C
  - Air Drying: 3 months with two months above 0 C
  - Anaerobic Digestion: 15 days @ 35-55 C no less than 60 days at 20 C
  - Composting: Minimum 40 C for 5 days with min 4 hours at 55 C
  - Lime Stabilization: Add lime to raise pH to 12 after two hours of contact
  - Other as approved by EPA Region 8




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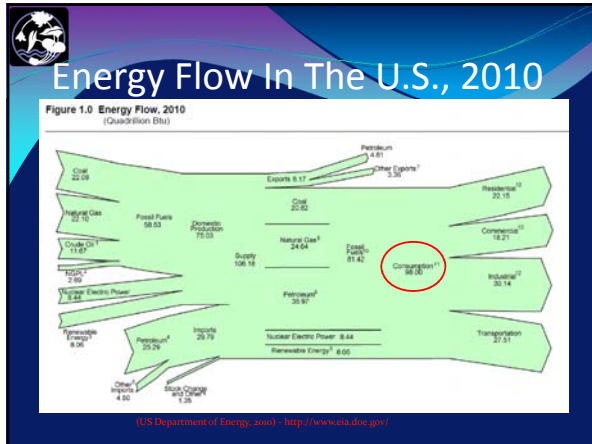
## MWRD - Metro Wastewater Reclamation District

- MetroGro
- About 52,000 dryland farm and pasture acres where they apply biosolids.
- Crop variety includes winter wheat, sorghum/sudan grass, and corn.
- Pasture areas are often used for sheep and cattle grazing.



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## Putting it into perspective

- 2010 Energy Consumption was 98 Quadrillion BTUs
- 98,000,000,000,000 BTUs (15 zeros!)
- 1 MW = 3414425 BTUs per hour
- 98 Quad BTU's is then about 3,276,456 MW
- Totals from previous slides is 17,835 MW
- About 0.5% of our total energy use each year

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### Example #1 – Seasonal CHP and Boiler Operation

- Site: Rochester Water Reclamation Plant
- Location: Rochester, MN
- Began Operation: 1982
- Operation Description:
  - 24 MGD wastewater treatment facility utilizing anaerobic digesters
- Project Description:
  - Biogas is utilized seasonally in
    - CHP system (2 MW capacity)
    - Boilers

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### Example #3 – Biogas Heating for Drying Biofibers

- Site: Geerlings Hillside Farms
- Location: Overisel, MI
- Began Operation: 2008
- Project Developer: Phase 3 Renewables
- Operation Description: Swine Farm with 8,000 spaces wean to finish
- Project Description: Anaerobic digestion
  - Biogas utilized in two (2) 65 kW engines (CHP system) and one (1) 1 MMBtu Boiler
  - Recovered heat from engines and heat from boilers is used to dry biofibers to enable pelletization
  - Pellet mill can produce 1.5 tons per hour; pellets can be used for fertilizer, boiler fuel or horse bedding

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### Example #5 – Gasification for Air Turbine and Steam

- Site: Sietsema Farms Feeds
- Location: Howard City, MI
- Began Operation: 2009
- Project Developer: Phase 3 Renewables
- Operation Description: Turkey Grower & Feed Mill
  - 1.5 million birds, five separate farm sites, 11,000 tons litter
  - Feed mill produces feed for turkeys and swine
- Project Description: Gasification, Electricity Generation, Heat and Steam
- Heat Application:
  - Syngas produced in SALT gasification facility
  - Advanced ceramic heat exchanger recovers air for use in 500kW air turbine generator
  - Metal heat exchanger recovers heat for 8,600 lbs/hr steam @ 150 psig for feed pelleting process

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## Europe Takes the Lead

- Europe has about 200 biogas plants in the early 1990's
- Today they have more than 16,000
- 60% are located in Germany
- Estimated to have 30,000+ by year 2015
- Older models only about 28% efficient or less

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**2G CENERGY**  
Advanced Clean Energy Technologies

A smart, less complicated  
and much more Cost-Effective Solution



The Solution for 2010 and beyond:

- High Efficiency & Biogas optimized
- Intelligent and very functional Design
- Small Footprint and easy Access
- Limited Space Requirements for Inside Installations
- Smart Container Module Design
- Maintenance Friendly, low Service Cost
- Extended Life Cycle & very Cost-effective



## Other Applications for Biogas

- Syngas – gasification of biomass
- Hydrogen Production from Methane
- Fuel Cells

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